

Thermodynamic Conservation of Energy

- 1st law of thermodynamics: E can't be created nor destroyed
- E changed from 1 form $\rightarrow$ another (heat $\rightarrow$ work).

Internal Energy - U

$U = \text{Total Energy} = \sum E_k + E_{\text{vib}} + E_{\text{rotational}}$

For a closed system:

- E given out by system = E gained by surroundings.
- E gained by system = E lost by surroundings.
- E either Heat (q) or Work (w)

closed system: change in $[U = \Delta U = q + w] = \text{heat} + \text{work}$.

Isolated system: $\Delta U = 0$ $\therefore q + w = 0$

Absolute value $U = \text{undetermined}$ - only measure differences (ΔU)

Assign E of particular state (standard state) to 0.

Experimental Measurement of ΔU

Constant volume calorimeter.

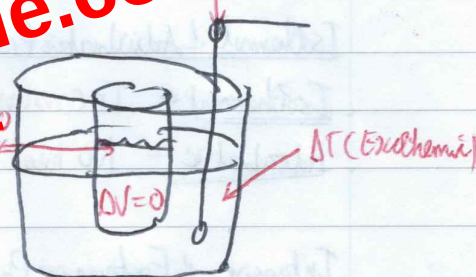
Pressure vessel (bomb) - standard cell with $U = \text{Calorimeter}$.

Temp. from both water baths - @ same temp.

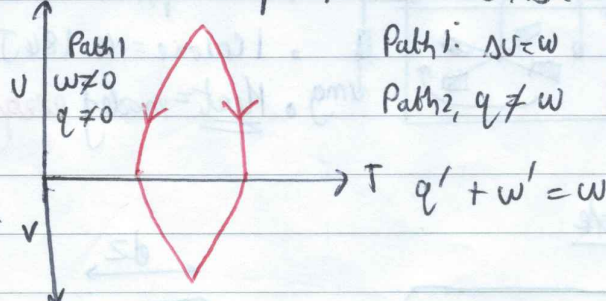
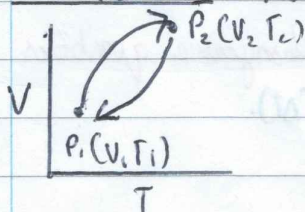
No net heat loss from calorimeter to outer water bath - calorimeter = adiabatic.

$\Delta T \propto q$ - Releases/absorbs heat; Calibrate calorimeter.

Burn known mass (Benzoin acid) & measure $\Delta T \rightarrow$ obtain c .



State Functions - Described by variables such as temp., pressure, V , S , ΔH etc.



$\sum (SF) = \sum (SF)_{\text{products}} - \sum (SF)_{\text{reactants}}$

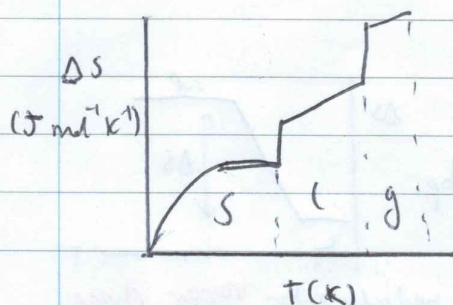
$\Delta U = \text{same}$ for both paths but values of w & w' & q & $q' = \text{different}$.

Change in state depends only on initial & final states & not on any intermediate conditions.
- Conservative force.

Boiling Pt & IMFs

Intro

Take ~~an~~ a state transition for ~~an~~ a substance, e.g. Tantalum.



$$\Delta G = \Delta H - T\Delta S$$

at EQ at some T $\Delta G = 0$, $\Delta H = T\Delta S$

$$\therefore \Delta S = \frac{\Delta H}{T}$$

$$S \rightleftharpoons L, \Delta_{\text{fus}} S = \frac{\Delta_{\text{fus}} H}{T}$$

$$L \rightleftharpoons G, \Delta_{\text{vap}} S = \frac{\Delta_{\text{vap}} H}{T}$$

When $\Delta_{\text{fus}} H$ & $\Delta_{\text{vap}} H > 0$, heat ~~absorbed~~ from surroundings.

When $\Delta_{\text{fus}} S$ & $\Delta_{\text{vap}} S > 0$, ~~entropy~~ goes from $L \rightarrow S$

Troun's rule

For a wide range of liquids, $\Delta_{\text{vap}} S = \frac{\Delta_{\text{vap}} H}{T} \approx 85 \text{ J mol}^{-1} \text{K}^{-1}$

Unless compounds with weak IMFs or T H bonding.

- Can be used to estimate $\Delta_{\text{vap}} H$ at constant T .
- Why? Because high disorder is generated when any liquid evaporates $\rightarrow$ become vapour.
- This disorder = comparable for many liquids.
- Therefore all liquids expected to have similar values of $\Delta_{\text{vap}} S^\circ$.

- Liquids that don't obey Troun's rule do so as they're arranged to be more ordered.
- So ΔS = greater (greater change of disorder) occurs on evaporation
- For H-bonded liquids, H bonds organise ~~the~~ molecules so they're less random than others.

Reactions at EQ: Exergonic & Endergonic

When a reaction has reached EQ ($\Delta G = 0$), $\Delta_r G^\ominus = RT \ln K$.

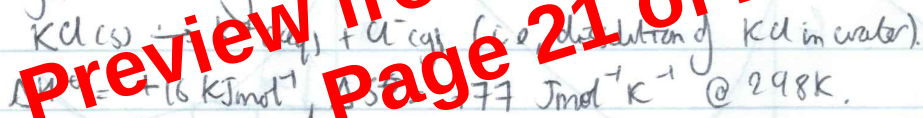
- Exergonic: $K > 1$ if $\Delta_r G^\ominus < 0$ & $\Delta S^\ominus > 0$; i.e. products in excess $\Rightarrow$ Reaction thermodynamically feasible.
- Endergonic: $K < 1$ if $\Delta_r G^\ominus > 0$ & i.e. reactants in excess $\Rightarrow$ Reaction Not thermodynamically feasible.

NB: $K \gg 1$ to have significantly more product than reactant.

Conditions when $K > 1$ & $\Delta_r G^\ominus < 0$, Consider $\Delta_r G^\ominus = \Delta_r H^\ominus - T \Delta_r S^\ominus$

- 1) $\Delta_r H^\ominus < 0$ & $\Delta_r S^\ominus > 0$, $\Rightarrow \Delta_r G^\ominus < 0$, non-Exergonic.
- 2) $\Delta_r H^\ominus < 0$ & $\Delta_r S^\ominus < 0$ provided $(T < \Delta_r H^\ominus / \Delta_r S^\ominus) \Rightarrow \Delta_r G^\ominus < 0$.
- 3) $\Delta_r H^\ominus > 0$ & $\Delta_r S^\ominus > 0$ provided $(T > \Delta_r H^\ominus / \Delta_r S^\ominus) \Rightarrow \Delta_r G^\ominus < 0$.
- 4) $\Delta_r H^\ominus > 0$ & $\Delta_r S^\ominus < 0 \Rightarrow \Delta_r G^\ominus > 0$ for all temps.

E.g. For an exergonic reaction:



Using 3) above, $298 \text{ K} > \frac{16000 \text{ kJ mol}^{-1}}{77 \text{ J mol}^{-1} \text{ K}^{-1}} = 207.8 \text{ K (Thre)}$ $T = \frac{\Delta_r H^\ominus}{\Delta_r S^\ominus}$

$$\Delta_r G^\ominus = \Delta_r H^\ominus - T \Delta_r S^\ominus = 16000 - (298.15 \times 77) = -7 \text{ kJ mol}^{-1}$$

i.e. $\Delta_r G^\ominus < 0$ so this reaction goes!

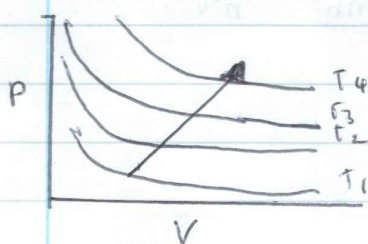
IMFs & VDW

- Need Ideal Gas Assumptions: $V(\text{of molecules}) \approx 0 \text{ m}^3$, no interactions between gas molecules.
- $P = nRT$, $P = \frac{nRT}{V}$, $P \propto \frac{1}{V}$ at T .

• Isotherms show the way P changes with V @ constant T .

• No liquid phase.

• $T_4 > T_1$ etc.



✓ Ideal Gas EQN Isotherms.

Real Gases

- Atoms/molecules of gas occupy some V , and
- Attractive & Repulsive interactions exist between gas molecules.
- If this was not true, all gases (e.g. H_2)

• We incorporate all this into the VDW equation

$$P = \frac{nRT}{V}$$

• Introduce a & b as proportionality constants

• nb = volume of molecules.

• $\frac{an^2}{V^2}$ = attractive terms proportional to momentum transferred, frequency of collisions.

$$P = \frac{nRT}{V-nb} - \frac{an^2}{V^2}$$

Mathematical Tweaks

n = no. of molecules, b = volume of molecules.

(i) Undefined = $V = nb$

(ii) Cubic equation in V : $P = f(V^3, V^2, V, 1)$.